

Caloric Properties from Empirical Fundamental Equations of State

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For well measured, technically and scientifically relevant fluids and fluid mixtures empirical multiparameter formulations in form of fundamental equations of state have been established as reference for thermodynamic properties. Well known examples for reference equations of state are those for carbon dioxide¹, nitrogen², and water³ – equations of state for fluids with excellent data sets, which are frequently applied not only in technical applications but also for calibration purposes. A number of fluids that are only relevant for technical applications are described with very high accuracy today, too; in particular this is true for some refrigerants⁴. Among the mixture models, the development of accurate property models based on multiparameter fundamental equations of state has focused on natural gas⁵ and CO₂-rich⁶ mixtures. Some of these models were formally accepted as international standards^{7,8}, others have been established as de facto standards by the scientific community and by internationally used software products⁹.

The drawback of empirical multiparameter equations of state is that they can only achieve high accuracy for fluids, for which accurate experimental data are available. Studies on suitable mathematical structures for fundamental equations of state, the use of algorithms optimizing their mathematical structure, and finally the use of constraints in nonlinear fitting⁴ have significantly improved the numerical stability of multiparameter equations of state¹⁰. They extrapolate well and yield reasonably accurate results in (limited) regions without data as well. However, multiparameter equations of state still depend on the availability of accurate experimental data in broad ranges of states, and estimates for the uncertainty of property values calculated from such equations can only be established by comparison to experimental data.

A crucial advantage of fundamental equations of state is that values for all thermodynamic properties are calculated from derivatives or from a combination of derivatives of a single surface spanning over temperature and density, respectively over temperature, density and composition for mixtures. Different properties calculated from a fundamental equation of state are not necessarily accurate, but they are always consistent to each other. As a consequence, fundamental equations of state can be based on data for those properties that can be measured with highest accuracy.

¹ R. Span and W. Wagner: A new equation of state for carbon dioxide covering the fluid region from the triple point temperature to 1100 K at pressures up to 800 MPa. *J. Phys. Chem. Ref. Data* 25, 1509 - 1596 (1996).

² R. Span, E. W. Lemmon, R. T Jacobsen, W. Wagner and A. Yokozeki: A reference equation of state for the thermodynamic properties of nitrogen for temperatures from 63.151 K to 1000 K and pressures to 2200 MPa. *J. Phys. Chem. Ref. Data*, 29, 1361 - 1433 (2000).

³ W. Wagner and A. Prueß: The IAPWS formulation 1995 for the thermodynamic properties of ordinary water substance for general and scientific use. *J. Phys. Chem. Ref. Data* 31, 387 - 535 (2002).

⁴ E. W. Lemmon and R. T Jacobsen: A new functional form and new fitting techniques for equations of state with application to pentafluoroethane (HFC-125). *J. Phys. Chem. Ref. Data* 34, 69 - 108 (2005).

⁵ O. Kunz and W. Wagner: The GERG-2008 wide-range equation of state for natural gases and other mixtures: An expansion of GERG-2004. *J. Chem. Eng. Data* 57, 3032 - 3091(2012).

⁶ J. Gemert and R. Span: EOS-CG: A Helmholtz energy mixture model for humid gases and CCS mixtures. *J. Chem. Thermodyn.* 93, 274 - 293 (2016).

⁷ *International Association for the Properties of Water and Steam (IAPWS)*: Revised release on the IAPWS formulation 1995 for the thermodynamic properties of ordinary water substance for general and scientific use (2014).

⁸ *International Organization for Standardization (ISO)*: ISO 20765-2:2015, Natural gas - Calculation of thermodynamic properties - Part 2: Single-phase properties (gas, liquid, and dense fluid) for extended ranges of application (2015).

⁹ E. W. Lemmon, M. L. Huber, and M. O. McLinden: NIST Standard Reference Database 23: Reference fluid thermodynamic and transport properties - REFPROP, version 9.1. National Institute of Standards and Technology, Standard Reference Data Program, Gaithersburg, 2013.

¹⁰ R. Span and W. Wagner: On the extrapolation behavior of empirical equations of state. *Int. J. Thermophys.*, 18, 1415 - 1443 (1997).

Today, multiparameter fundamental equations of state are mostly based on density and speed of sound data at homogeneous states. Highly accurate equipment for density^{11,12} and speed of sound^{13,14} measurements has been developed to provide the required data for pure fluids and mixtures. Beside this, accurate information on vapour-liquid equilibria is mandatory to precisely describe the location of the phase boundary. Extensive data sets have been provided for pure reference fluids and a number of mixtures.

Experience shows that fundamental equations of state based on highly accurate density and speed of sound data describe caloric properties like heat capacities more accurately than the available experimental data. For diluted gas states this statement and its limits can easily be proven. However, for higher density and correspondingly large residual effects these relations become more complex. To date it is not possible to base traceable uncertainty statements for caloric properties on deviations observed for densities or speeds of sound. Mathematical approaches can be derived, but to verify or to falsify their applicability, comprehensive sets of highly accurate data for heat capacities or enthalpy differences would be required at least for some reference fluids.

¹¹ *R. Kleinrahm and W. Wagner*: Measurement and correlation of the equilibrium liquid and vapour densities and the vapour pressure along the coexistence curve of methane. *J. Chem. Thermodynamics* 18, 739 – 760 (1986).

¹² *M. Richter, R. Kleinrahm, R. Lentner, and R. Span*: Development of a special single-sinker densimeter for cryogenic liquid mixtures and first results for a liquefied natural gas (LNG). *J. Chem. Thermodyn.* 93, 205 - 221 (2016).

¹³ *J.P.M. Trusler and M. Zarari*: The speed of sound and derived thermodynamic properties of methane at temperatures between 275 K and 375 K and pressures up to 10 MPa. *J. Chem. Thermodyn.* 24, 973 – 991 (1992).

¹⁴ *K. Meier and S. Kabelac*: Speed of sound instrument for fluids with pressures up to 100 MPa. *Rev. Scien. Instrum.* 77, 123903 - 123908 (2006).